Dry reforming of methane for syngas production over Ru catalysts supported on mixed $CeO_2 - M_2O_3$ oxides (M: La, Pr, Nd, Eu, Gd, Tb, Dy, Er)

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The European Union has pledged to reach carbon neutrality by 2050 harnessing renewable energy sources that have enormous potential as fossil fuel alternatives. Among many, like solar, wind or tidal, biogas is a promising factor in decarbonizing our energy systems. Biogas is composed mainly by CH₄, CO₂, two relatively inert gases that could be utilized to either produce hydrogen or synthetic fuels [1,2]. The Dry Reforming of Methane (DRM) reaction to produce syngas (H₂ and CO) has been gaining increasing popularity over the years in the scientific community compared to the Steam Reforming of Methane (SRM) reaction or the Partial Oxidation of Methane (POM) reaction. This is attributed to the advantages that DRM offers in comparison with the two alternative reforming reactions, namely the valorization of the two most important greenhouse gases (CH₄, CO₂), the production of syngas with a H₂/CO ratio close to unity which renders it ideal for Fischer-Tropsch reactions to produce synthetic fuels, as well as the ability to directly use biogas deriving from anaerobic digestion of biomass from landfills or sewage refining facilities, which is composed of 50-70 % CH₄ and 25-50 % CO₂ [3,4]. Of great importance, when it comes to the yield of the DRM reaction using supported metallic catalysts, is the nature of the support and the promoters employed. The promotion of Cerium oxide (CeO₂) with rare earth elements (e.g. Pr) improves the ability of CeO_2 to store oxygen [5] but also the lability of the lattice oxygen, thereby diminishing the carbon formed on the surface of the catalyst and facilitating the activation of CO₂. Toward this direction a series of 1 wt.% Ru catalysts supported on mixed oxides $Ce_{0.8}M_{0.2}O_x$ (M: La, Pr, Nd, Eu, Gd, Dy and Er) were synthesized by the wet impregnation method in order to be studied as it concerns their DRM activity. The supports were synthesized via the coprecipitation method [6] with a molecular ratio of Ce:M equal to 80:20. The as synthesized catalysts were characterized with respect to their specific surface area and phase composition employing the BET method and X-ray diffraction technique, respectively. The reducibility of the catalysts was investigated with the TPR-H₂ technique. The catalytic performance tests were performed in the temperature range 550-800 °C with a volumetric feed ratio of CH₄: CO₂ equal to 50:50. Ru catalysts supported on Ce_{0.8}Dy_{0.2}O_x and $Ce_{0.8}Gd_{0.2}O_x$ mixed oxide carriers have shown the best results.

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